

CONCLUSIONS

In this paper the ground temperature $T(x,t)$ due to arbitrary solar temperature is expressed in terms of response function and the convolution integral. Analytic solution of the integral is obtained for periodic variation of $T_A(t)$. The resulting expression for $T(x,t)$ is found to be same as that obtained by periodic analysis by earlier authors. The equivalence of two methods for a periodic input is used to determine the preceding significant time in response function method. Subsequently the results of response function analysis and the periodic analysis are compared for a cloudy day preceded by cloudy days.

Acknowledgements — Our sincere thanks are due to Prof. M. S. Sodha for suggestion of the problem and help at various

stages of the work. Thanks are due also to Dr. C. L. Gupta for discussion.

REFERENCES

1. E. R. G. Eckert and D. N. Drake, *Heat and Mass Transfer*. McGraw-Hill, New York (1959).
2. A. K. Khatri, M. S. Sodha and M. A. S. Malik, *Sol. Energy* **20**, 425 (1978).
3. N. K. D. Chaudhry and Z. U. A. Warsi, Weighting function and transient thermal response of buildings, *Int. J. Heat Mass Transfer* **7**, 1309 (1964).
4. G. P. Mitalab and D. G. Stephenson, Room thermal response factors, *Trans. ASHRAE*, Paper 2019 (1967).

Int. J. Heat Mass Transfer. Vol. 23, pp. 906-908
Pergamon Press Ltd. 1980. Printed in Great Britain

BEHAVIOUR OF THE TURBULENT PRANDTL NUMBER NEAR THE WALL

R. A. ANTONIA

Department of Mechanical Engineering, University of Newcastle,
New South Wales 2308, Australia

(Received 2 October 1978 and in revised form 10 January 1980)

NOMENCLATURE

Pr ,	molecular Prandtl number $\equiv \nu/\gamma$;
Pr_t ,	turbulent Prandtl number $\equiv (uv \partial T/\partial y)/$ $(v\theta \partial U/\partial y)$;
Q_w ,	thermometric wall heat flux;
R_{uw} ,	correlation coefficient $\overline{uw}/(\overline{u^2}^{1/2} \overline{w^2}^{1/2})$;
$R_{v\theta}$,	correlation coefficient $\overline{v\theta}/(\overline{v^2}^{1/2} \overline{\theta^2}^{1/2})$;
T ,	local mean temperature;
T_w ,	wall temperature;
T_τ ,	friction temperature Q_w/U_τ ;
T^+ ,	$(T_w - T)/T_\tau$;
U, V ,	mean velocities in x, y directions, respectively;
U_τ ,	friction velocity $= \tau_w^{1/2}$;
U^+ ,	ratio U/U_τ ;
u, v, w ,	velocity fluctuations in x, y, z directions, respectively;
u^+, v^+, w^+ ,	$u/U_\tau, v/U_\tau$ and w/U_τ , respectively;
$-\overline{u\bar{v}}$,	Reynolds shear stress;
$v\theta$,	turbulent heat flux;
x, y, z ,	space co-ordinates in streamwise, normal and spanwise directions;
y^+ ,	non-dimensional normal co-ordinate yU_τ/ν .

Greek symbols

α_i, β_i ,	coefficients in equations (1)–(4);
γ ,	thermal diffusivity;
δ_i ,	coefficients in equations (11)–(13);
θ ,	temperature fluctuation;
θ^+ ,	θ/T_τ ;
τ_w ,	kinematic wall shear stress;
ν ,	kinematic viscosity.

Subscript

w ,	denotes wall value.
-------	---------------------

INTRODUCTION

THE TREND of Pr_t in the region $0 < y^+ < 40$ and its possible dependence on Pr have not yet been established. Launder [1] suggested that the most sensible requirement is that any proposal of Pr_t in this region should lead to adequate predictions of measured mean temperature profiles and surface heat flux. In this context, Cebeci's [2] model indicates that, close to the wall, Pr_t increases as the wall is approached and remains constant within the viscous sublayer. The constant, as determined by Na and Habib [3] is approximately 1.43. Wassel and Catton [4] use a similar model for their calculation method, except that the constant is about 1.32, again for air. Sleicher [5] calculated Pr_t from measured velocity and temperature profiles of air in fully developed pipe flow and found that Pr_t approached a constant of about 1.4 very near the wall. This value is slightly higher than the value of $Pr_t^{-1/2}$ suggested, for example, by Sherwood *et al.* [6]. That Pr_t is constant, for a given Pr , very near the wall is verified by analytical considerations of mean velocity, mean temperature, Reynolds shear stress and mean heat-flux profiles in the region close to the wall. Considerations of this type have been given by Meroney [7] and Orlando *et al.* [8]. Meroney did not attempt to estimate the constant, but Orlando *et al.* suggested an experimental procedure that yields a value of about 1.4 for this constant. Although the actual value of Pr_t at the wall is not relevant to methods of calculating the heat transfer in a boundary layer, an accurate description of Pr_t in the buffer zone (approximately $5 < y^+ < 20$) can serve as a useful input to calculation methods. In the present note, the analysis followed in [7] and [8] is used with a view to establish the trend of Pr_t near the wall. This analysis is consistent with the Navier–Stokes and heat-transfer equations and yields a distribution of Pr_t , using available experimental mean velocity, temperature, momentum and heat flux profiles close to the wall.

ANALYSIS AND RESULTS

The behaviour of Pr_t near the wall can be inferred from Taylor series expansions (e.g., [7, 9, 10]) of uv , $v\theta$, U and T in terms of y , viz.,

$$\overline{u^+v^+} = \alpha_1 y^{+3} + \alpha_2 y^{+4} + 0(y^{+5}), \quad (1)$$

$$\overline{v^+\theta^+} = \alpha_3 y^{+3} + \alpha_4 y^{+4} + 0(y^{+5}), \quad (2)$$

$$U^+ = y^+ + \beta_1 y^{+4} + \beta_2 y^{+5} + 0(y^{+6}), \quad (3)$$

$$T^+ = Pr_t y^+ + \beta_3 y^{+4} + \beta_4 y^{+5} + 0(y^{+6}). \quad (4)$$

The constants α_i ($i = 1-4$) can be expressed as correlations at the wall between derivatives, with respect to y , of velocity and/or temperature fluctuations. These constants can be related to the corresponding β_i s if the total shear stress ($-uv + \nu \partial U / \partial y$) and total heat flux ($v\theta - \gamma \partial T / \partial y$) are assumed constant near the wall. The appropriate relations are $\alpha_1 = 4\beta_1$, $\alpha_2 = 5\beta_2$, $\alpha_3 = -4Pr_t^{-1}\beta_3$, $\alpha_4 = -5Pr_t^{-1}\beta_4$. At the wall, Pr_t can be written, using equations (1)–(4), as

$$Pr_t = \frac{\alpha_1 Pr}{\alpha_3} = \frac{\beta_1}{\beta_3} Pr^2. \quad (5)$$

This expression, identical to that obtained in [7] (it can also be derived from the results of [9] and [10]), indicates that for a given Pr , Pr_t is constant at the wall. The numerical value of the constant can be obtained from a knowledge of β_1 and β_3 .

Values of α_1 , α_2 , β_1 – β_4 may be obtained from least squares regressions of equations (1), (3) and (4) using available experimental data of $\overline{u^+v^+}$, U^+ and T^+ in the wall region. Measurements of $\overline{v^+\theta^+}$ do not seem to be available close to the wall and hence it is not possible to obtain an independent check of the relations between α_3 (or α_4) and β_3 (or β_4). Values of α_i , β_i are shown in Table 1 using the data ($0 < y^+ < 20$) of Eckelmann [11] who made measurements in a two-dimensional oil channel with a thick viscous sublayer and of Blom [12] who made measurements in a boundary layer downstream of a step in surface temperature. Use was also made of Laufer's [13] data to determine α_1 and α_2 . Also shown in the table are α_1 values obtained by Townsend [14] and Coantic [15] who considered the $\overline{u^+v^+}$ data of Laufer [13] and Klebanoff [16]. It is interesting to note that Hinze [17] estimated α_1 to be of order 10^{-4} from a knowledge of measured RMS values of $(\partial u^+ / \partial y^+)$ and $(\partial w^+ / \partial y^+)$ at the wall and the experimental observation that the spanwise separation z^+ of longitudinal streaks observed close to the wall is about 100. Another way of estimating the β s is to

match equations (3) and (4) with the expressions for U^+ and T^+ in the buffer region. These estimates (see Table 1) are in reasonable agreement with those obtained from least squares regressions to the sublayer data. The average values of β_1 – β_4 are -1.6×10^{-4} , 5.8×10^{-6} , -1.4×10^{-4} and 5.6×10^{-6} respectively. With these values, equation (5) yields $Pr_t = 0.61$. Near the wall, the behaviour of Pr_t , for air, can be approximated by

$$Pr_t \approx 0.61 \frac{(1 - 0.045y^+)}{(1 - 0.05y^+)}, \quad (6)$$

so that Pr_t has zero slope at the wall and increases sharply near the edge of the sublayer. This is in contrast with the trend in [2, 4, 8] where Pr_t decreases sharply near the edge of the sublayer from a constant value of about 1.4 near the wall. Equation (6) would be consistent with a variation of Pr_t that exhibits a peak near the edge of the sublayer before decreasing toward a constant value of about 0.9 for $y^+ > 40$. Such a trend would be compatible with that suggested by (1) and (18), and in agreement with the Pr_t variation prescribed for one of the calculation methods considered in [19].

A further indirect check of α_1 (or β_1) and α_3 (or β_3) may be obtained by considering the behaviour of the correlation coefficients R_{uv} and $R_{v\theta}$ near the wall. Distributions of $u^{2+1/2}$ and $v^{2+1/2}$ in the region close to the wall may be written as (e.g. [15], p. 220)

$$\overline{u^{+2+1/2}} = \delta_1 y^+ + \delta_2 y^{+2} + 0(y^{+3}), \quad (7)$$

$$\overline{v^{+2+1/2}} = \delta_3 y^{+2} + \delta_4 y^{+3} + 0(y^{+4}). \quad (8)$$

It is relatively easy to show that, near the wall, $\overline{\theta^{+2+1/2}}$ is given by

$$\overline{\theta^{+2+1/2}} = \delta_5 y^+ + \delta_6 y^{+3} + 0(y^{+4}). \quad (9)$$

The coefficients δ_i , inferred from experimental contributions of these RMS quantities close to the wall, are included in Table 1. Using average values of δ_1 , δ_3 , δ_5 of 0.30, 7.4×10^{-3} , 0.17 and with $\alpha_1 = -5.5 \times 10^{-4}$ and $\alpha_3 = 7.7 \times 10^{-4}$ ($= -4Pr_t^{-1}\beta_3$ with $Pr = 0.73$), the correlation coefficients R_{uv} and $R_{v\theta}$ are 0.25 and 0.61, respectively, at the wall. These values do not seem unreasonable in the light of the trend of Fulachier's [21] data for R_{uv} and $R_{v\theta}$ close to the wall.

Acknowledgement—The support of the Australian Research Grants Committee is gratefully acknowledged. The author is also grateful to Dr. L. W. B. Browne for helpful comments on the manuscript.

Table 1. Coefficients α_i , β_i , δ_i

Investigator	Data	α_1 ($\times 10^4$)	α_2 ($\times 10^5$)	β_1 ($\times 10^4$)	β_2 ($\times 10^6$)	β_3 ($\times 10^4$)	β_4 ($\times 10^6$)	δ_1	δ_3 ($\times 10^3$)	δ_5
Present	[11]	-5.5	2.3	-1.7 (-1.6)†	6.1 (6.4)				6.3	
Present	[12]			-1.4	4.8	-1.4 (-1.4)	5.3 (6)			0.19
Present	[13]								8.6	
Townsend [14]		-6						0.3	9.2	
Coantic [15]	[13, [16]	-11							8	
Elena [20]								0.3		0.15

† Values in brackets are obtained by matching to the buffer region.

REFERENCES

1. B. E. Launder, Heat and mass transport, in *Topics in Applied Physics*, Vol. 12, p. 231. Springer, Berlin (1976).
2. T. Cebeci, A model for eddy conductivity and turbulent Prandtl number, *J. Heat Transfer* **95**, 227–234 (1973).
3. T. Y. Na and I. S. Habib, Heat transfer in turbulent pipe flow based on a new mixing length model, *Appl. Scient. Res.* **28**, 302–314 (1973).
4. A. T. Wassel and I. Catton, Calculation of turbulent boundary layers over flat plates with different phenomenological theories of turbulence and variable turbulent Prandtl number, *Int. J. Heat Mass Transfer* **16**, 1547–1563 (1973).
5. C. A. Sleicher, Jr., Experimental velocity and temperature profiles for air in turbulent pipe flow, *J. Heat Transfer* **80**, 693–704 (1958).
6. T. K. Sherwood, K. A. Smith and P. E. Fowles, The velocity and eddy viscosity distribution in the wall region of turbulent pipe flow, *Chem. Engng. Sci.* **23**, 1225–1234 (1968).
7. R. N. Meroney, Turbulent sublayer temperature distribution including wall injection and dissipation, *Int. J. Heat Mass Transfer* **11**, 1406–1408 (1968).
8. A. F. Orlando, R. J. Moffat and W. M. Kays, Turbulent transport of heat and momentum in a boundary layer subject to deceleration, suction and variable wall temperature, Report No. HMT-17, Thermosciences Div., Dept. Mech. Engng., Stanford University (1974).
9. C. L. Tien, A note on distributions of temperature and eddy diffusivities for heat in turbulent flow near a wall, *Z. Angew. Math. Phys.* **15**, 63–66 (1964).
10. C. L. Tien and D. T. Wassan, Law of the wall in turbulent channel flow, *Physics Fluids* **6**, 144–145 (1963).
11. H. Eckelmann, The structure of the viscous sublayer and the adjacent wall region in a turbulent channel flow, *J. Fluid Mech.* **65**, 439–459 (1974).
12. J. Blom, An experimental determination of the turbulent Prandtl number in a developing temperature boundary layer, Ph.D. Thesis, Technological University, Eindhoven (1970).
13. J. Laufer, The structure of turbulence for a fully developed pipe flow, NACA TR1174 (1954).
14. A. A. Townsend, *The Structure of Turbulent Shear Flow*. Cambridge University Press, Cambridge (1956).
15. M. Coantic, Contribution à l'étude de la structure de la turbulence dans une conduite de section circulaire, Thèse Docteur ès Sciences, Université d'Aix-Marseille (1966).
16. P. S. Klebanoff, Characteristics of turbulence in a boundary layer with zero pressure gradient, NACA Report 1247 (1955).
17. J. O. Hinze, *Turbulence*, p. 621. McGraw-Hill, New York (1975).
18. E. M. Khabakhpasheva and B. V. Perepelitsa, Measurements of temperature, velocity fields and turbulent Prandtl number in near-wall flow region, in *Proceedings 5th International Heat Transfer Conference*, p. 134, Tokyo (1974).
19. L. W. B. Browne and R. A. Antonia, Calculation of a turbulent boundary layer downstream of a step change in surface temperature, *J. Heat Transfer* **101**, 144–150 (1979).
20. M. Elena, Etude expérimentale de la turbulence au voisinage de la paroi d'un tube légèrement chauffé, *Int. J. Heat Mass Transfer* **20**, 935–944 (1977).
21. L. Fulachier, Contribution à l'étude des analogies des champs dynamique et thermique dans une couche limite turbulente, Thèse Docteur ès Sciences, Université de Provence, Marseille (1972).